

Catalytic properties of novel La–Sr–Cu–O–S perovskites for automotive C₃H₆/CO oxidation in the presence of SO_x

M. Machida^{*}, K. Ochiai, K. Ito, K. Ikeue

*Department of Applied Chemistry and Biochemistry, Faculty of Engineering, Kumamoto University,
2-39-1 Kurokami, Kumamoto 860-8555, Japan*

Available online 11 July 2006

Abstract

A La–Sr–Cu–O–S system with K₂NiF₄ perovskite-type structure has been studied as a novel SO_x-resistant combustion catalyst. The XRD result implied that sulfur is incorporated into the structure as non-sulfate-type cations. An introduction of sulfur with highly positive valence (S⁶⁺ or S⁴⁺) into the lattice requires the charge compensation by decreasing the oxidation number of Cu. This is accompanied by the creation of more reducible Cu species, which would achieve the light-off of catalytic C₃H₆ oxidation at lower temperatures. More important feature of sulfur-containing compounds is that the catalytic C₃H₆ oxidation was significantly accelerated by addition of SO₂ to the gas feed. The catalytic performance for the oxidation of C₃H₆ and CO and the reduction of NO was finally evaluated in a simulated automotive exhaust in the presence of SO₂.

© 2006 Elsevier B.V. All rights reserved.

Keywords: Perovskite; Sulfur; Oxidation; Redox; Cu; C₃H₆

1. Introduction

Metal oxides with perovskite-type structure have extensively been studied as alternatives to noble metal catalysts for automotive emission control since 1970s [1]. The compounds which contain Mn or Co in the B-site of the perovskite structure are known as one of most active catalysts for the oxidation of hydrocarbons as well as CO. However, a serious problem is deactivation due to sulfur (SO₂) poisoning, because solid–gas reactions between SO₂ and perovskites are inevitable at high temperatures. Because many perovskite oxides contain alkaline earth or rare earth metals with a high basicity, the formation of sulfates from oxides is thermodynamically favorable in a wide temperature range. Several attempts have been made so far to overcome this problem by introducing Ru or Pt oxide less sensitive to SO₂ poisoning [2–4] and MgO as preferential adsorption site for SO₂ [5], or by seeking for sulfur bearing catalyst compositions [6–8]. Nevertheless, the development of SO₂-resistant perovskite catalysts remains unsolved even in the present stage. For the reason, a novel approach to design SO_x-

resistant perovskite catalysts is strongly requested. In the present study, K₂NiF₄-type perovskite-related compounds, La–Sr–Cu–O–S, have been studied as a novel SO₂-resistant catalyst material. The effect of SO₂ in catalytic C₃H₆/CO oxidation was evaluated not only in a microreactor but also in an automotive-simulated reactor.

2. Experimental

La_{2–x}Sr_xCuO₄S_y (0 ≤ x ≤ 0.3, 0 ≤ y ≤ 0.3) compounds were synthesized by calcining stoichiometric mixtures of La₂O₃, SrCO₃, CuO, and CuSO₄ at 950 °C in air. The characterization was done by XRD, XRF, IR, XPS, TG, and TPR. The TPR measurement was conducted in a conventional flow reactor connected to a differential evacuation system. After evacuation at ambient temperature, the sample was heated in a flowing gas mixture of 10% H₂ and He (20 cm³ min^{–1}) at a constant rate (10 °C min^{–1}) up to 950 °C. Effluent gas from the sample was analyzed by a quadrupole residual gas analyzer mass spectrometer. Catalytic oxidation of C₃H₆ was examined in a conventional flow reactor at atmospheric pressure. The light-off characteristic was evaluated in a microreactor by heating the catalysts (0.2 g) from room temperature to 800 °C at constant rate of 2 °C min^{–1} in a gaseous mixture of C₃H₆

^{*} Corresponding author. Tel: +81 96 342 3651, fax: +81 96 342 3651.

E-mail address: machida@chem.kumamoto-u.ac.jp (M. Machida).

(0.2%), O₂ (0.5 or 5%), and N₂ (balance) supplied at 100 cm³ min⁻¹ (W/F = 0.002 g cat. min cm⁻³). The sensitivity to SO₂ poisoning was evaluated during isothermal catalytic oxidation of C₃H₆ at ca. 400 °C by adding 20 ppm SO₂ to the gas feed and monitoring the change in C₃H₆ conversion to CO₂. Catalytic reactions were also carried out in a simulated automotive exhaust; 0.1% C₃H₆, 0.65% CO, 0.15% NO, 3% H₂O, 10 or 0.7% O₂, at space velocity (SV) of 200,000 h⁻¹.

3. Results and discussion

Perovskite oxides containing sulfur can be found in a series of studies directed toward high-temperature superconducting materials in 1990s. One example is the K₂NiF₄-type cuprate system, La_{1.85}Sr_{0.15}Cu_{1-x}O_{4-x}(SO₄)_x, in which sulfur is considered to be present in the form of sulfate ions (SO₄²⁻) substituting ca. 10% of Cu site [9]. Another compound, Ba₄YCu_xO₉(SO₄)_y, which was also reported to contain SO₄ units substituting part of the Cu site in the structure, can accommodate larger amounts of sulfur up to y = 0.8 [10]. Although these materials are thermally stable, the catalytic property, chemical state, and stability of sulfur species in the perovskite structure have not been studied so far.

Fig. 1 shows the XRD patterns of La_{2-x}Sr_xCuO₄S_{0.2} (0 ≤ x ≤ 0.3). As prepared compounds contained almost stoichiometric sulfur, but part of sulfur was deposited as La₂O₂SO₄ at lower x and as SrSO₄ at higher x. The composition with minimal impurities were determined to be x = 0.3. The diffraction pattern of the main phase is very similar to that of the La_{1.85}Sr_{0.15}Cu_{1-x}O_{4-x}(SO₄)_x [9], but our X-ray structural analysis by means of the Rietveld method led to a different conclusion [11]. Fig. 2 shows the crystal structure model of the product with y = 0 and 0.2. The structural parameters for y = 0 is very similar to that reported for this material [12], in which La and Sr are distributed randomly in the A-site. For y = 0.2, sulfur is located in the interstitial site between adjacent two

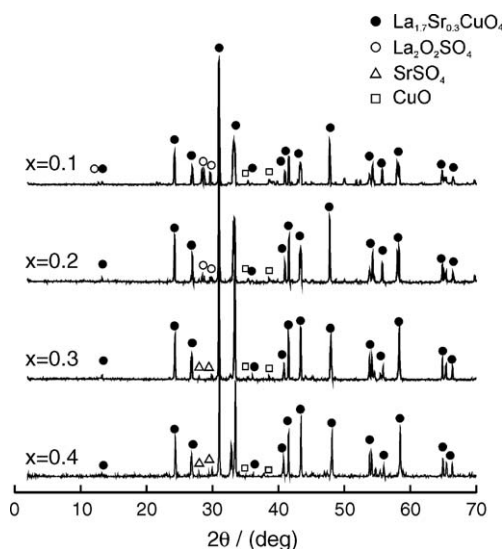


Fig. 1. XRD patterns of La_{2-x}Sr_xCuO₄S_{0.2} after calcination at 950 °C in air.

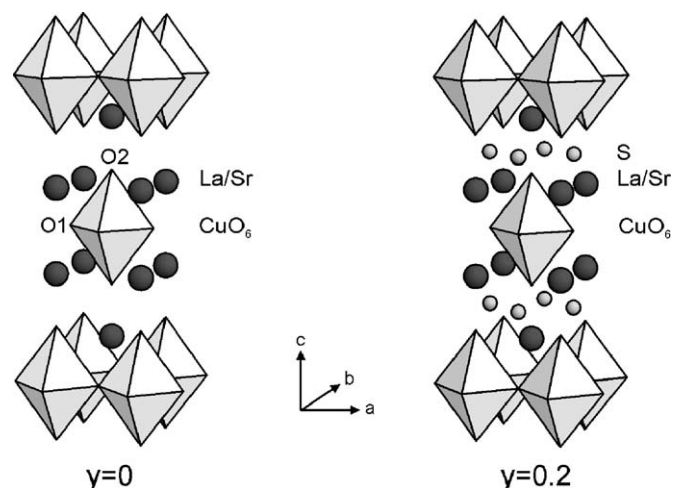


Fig. 2. Crystal structure of K₂NiF₄-type La_{1.7}Sr_{0.3}CuO₄ (y = 0) and La_{1.7}Sr_{0.3}CuO₄S_{0.2} (y = 0.2).

perovskite layers. Sulfur in this site is surrounded by four oxygens, but the S–O bond length (0.21 nm) is larger than that (0.15 nm) in a tetrahedral SO₄²⁻ ion. The compound contained about 50% of sulfur in the site in the K₂NiF₄ lattice, whereas other sulfur would be deposited as impurity (SrSO₄).

The XRD analysis of the present study suggests that sulfur in the K₂NiF₄-type cuprate is not a sulfate. This is consistent with FT-IR results with no obvious absorption due to SO₄ groups. The XPS measurement showed the S 2p signals (*E*_B = 169 and 167 eV) similar to S⁶⁺ and S⁴⁺. Although part of the S⁶⁺ signal comes from a SrSO₄ impurity, sulfur species in the structure should have highly positive valences. The TG analysis of La_{1.7}Sr_{0.3}CuO₄S_y in a flowing H₂ showed that the oxidation number of Cu was decreased with increasing the S content. This is reasonable because the positive valence of sulfur in the lattice would be compensated by the oxidation number of Cu.

Thermal evolution of lattice oxygen as O₂ was very small from as prepared cuprates. Thus, the reduction behavior was studied by means of H₂-TPR technique as shown in Fig. 3.

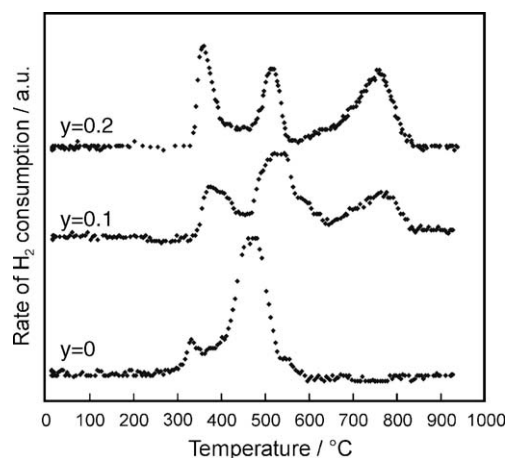


Fig. 3. TPR profiles of La_{1.7}Sr_{0.3}CuO₄S_y in a stream of 5% H₂/He. Heating rate: 10 °C min⁻¹.

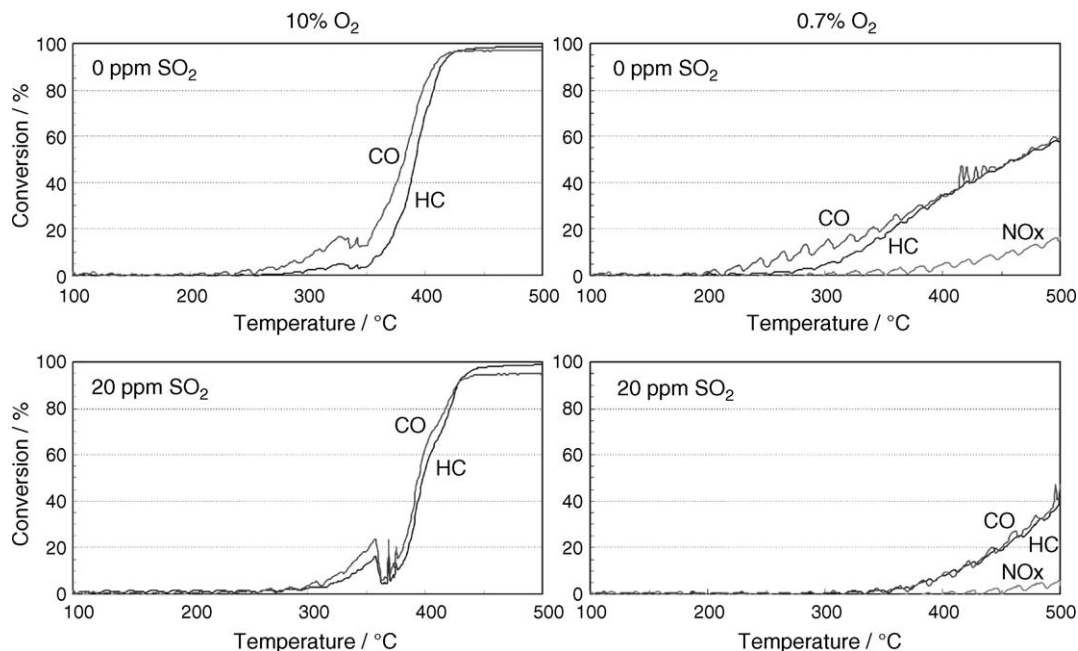


Fig. 4. Catalytic activity of the sulfur-containing phase ($y = 0.2$) for simulated automotive exhaust. 0.1% C_3H_6 , 0.65% CO, 0.15% NO, 3% H_2O , 10 or 0.7% O_2 , 0 or 20 ppm SO_2 ; SV = 200,000 h^{-1} .

When the pristine sample ($x = 0$) was heated in the stream of 10% H_2/He , two peaks due to H_2 consumption were observed at ca. 320 and 470 $^{\circ}C$. A small peak at 320 $^{\circ}C$ is ascribable to the reduction of Cu^{3+} to Cu^{2+} and a large peak is due to the reduction of Cu^{2+} to Cu^0 . The parallel XRD measurement indicated that the second peak was accompanied by the decomposition of K_2NiF_4 -type perovskite to a mixture of La_2O_3 , SrO , and Cu . On the contrary, the reduction peak split into two peaks at ca. 380 and 500 $^{\circ}C$ with an increase of the S content. This means that two Cu species with different reducibility were generated by introducing sulfur. Unlike the pristine compound, the sulfur-containing compound was decomposed into a mixture of La_2O_3 , $SrSO_4$, and Cu . This is the reason why another reduction peak appeared at higher temperature of ca. 760 $^{\circ}C$. The third peak can be assigned to the reduction of $SrSO_4$ (S^{6+}) to SrS (S^{2-}).

The catalytic activity of the sulfur-containing catalyst for the oxidation of C_3H_6 was carried out in a fixed bed microreactor. No significant change in the activity was observed irrespective of the sulfur content ($y \leq 0.2$). Nevertheless, the response to SO_2 was very interesting; the C_3H_6 conversion at 400 $^{\circ}C$ over sulfur-containing catalyst ($y = 0.2$) increased from 60 to more than 98% by supplying 20 ppm SO_2 in the presence of 5% O_2 . The activity was very stable so that the conversion was kept almost constant during 50 h. Considering the concentration of SO_2 (20 ppm) much less than C_3H_6 (0.2%), direct interaction between these two reactants unlikely occurred. The XPS analysis showed that the amount of SO_2 adsorption onto the sulfur-containing phase was less than that onto a pristine phase ($y = 0$). However, the SO_2 adsorption onto sulfur-containing compounds may produce the adsorption species effective in enhancing the conversion of C_3H_6 in an excess O_2 . A similar

catalytic activation caused by SO_2 was reported for propane oxidation over supported Pt catalysts and was explained by increased chemisorption of propane [13]. The effect of SO_2 on the chemisorption in the present system is now under investigation.

The catalytic performance was also evaluated in a simulated automotive exhaust at a high velocity of SV = 200,000 h^{-1} . Fig. 4 exhibits conversions of C_3H_6 , CO, and NO_x under lean (10% O_2) as well as stoichiometric (0.7% O_2) combustion conditions. Under a lean condition (10% O_2), steep rise in the conversion of C_3H_6 and CO occurred at >300 $^{\circ}C$, whereas the reduction of NO_x was scarcely observed. The deactivation in light-off characteristics was not caused by introducing 20 ppm SO_2 . In particular, the conversion of C_3H_6 in excess O_2 at ≤ 350 $^{\circ}C$ was rather gained by introducing SO_2 , which is consistent with the result in a microreactor. Under a stoichiometric condition (0.7% O_2), the conversions increased very gradually with an increase of temperature and the reduction of NO took place at ≥ 400 $^{\circ}C$. In this case, however, SO_2 caused the serious deactivation especially on the NO_x conversion.

4. Conclusions

The catalytic activity of sulfur-containing K_2NiF_4 -type cuprates was studied in the presence of SO_2 . The cationic sulfur in the lattice affected the oxidation state of Cu via the charge compensating mechanism. The activity of the sulfur-containing catalysts for C_3H_6 oxidation was found to be increased by SO_2 in an excess O_2 , whereas the effect disappeared at low O_2 concentrations. In a simulated automotive exhaust at a high velocity, however, the effect of sulfur in the perovskite structure became less obvious.

Acknowledgements

The present study was financially supported by a Grant-in-Aid for Scientific Research on Priority Area (440) from the Ministry of Education, Culture, Sports, Science and Technology (MEXT) and a Grant-in-Aid for Scientific Research from the Japan Society for the Promotion of Science (No. 16656250).

References

- [1] W.F. Libby, *Science* 171 (1971) 499;
R.J.H. Voorhoeve, J.P. Remeika, P.E. Freeland, B.T. Matthias, *Science* 177 (1972) 353;
R.J.H. Voorhoeve, J.P. Remeika, D.W. Johnson, *Science* 180 (1973) 62;
J.C. Schlatter, R.L. Klimisch, K.C. Taylor, *Science* 179 (1973) 797;
R.J.H. Voorhoeve, in: J.J. Burton, R.L. Garten (Eds.), *Advanced Materials in Catalysis*, Academic Press, New York, 1977, p. 129;
L.G. Tejuca, J.L.G. Fierro, J.M.D. Tascon, *Advances in Catalysis*, vol. 36, Academic Press, 1989, p. 237;
A. Cimino, F.S. Stone, *Adv. Catal.* 47 (2002) 141–306;
- A.T.V. Choudhary, S. Banerjee, V.R. Choudhary, *Appl. Catal. A: Gen.* 234 (2002) 1.
- [2] M. Shelef, H.S. Gandhi, *Plat. Met. Rev.* 18 (1975) 8.
- [3] L.E. Trimble, *Mat. Res. Bull.* 9 (1974) 1405.
- [4] J.S. Croat, G.G. Tibbetts, *Science* 194 (1976) 318.
- [5] I. Rosso, G. Saracco, V. Specchia, E. Garrone, *Appl. Catal. B: Environ.* 40 (2003) 195.
- [6] P.G. Tsyrlunikov, O.N. Kovalenko, L.L. Gogin, T.G. Starostina, A.S. Noskov, *Appl. Catal. A: Gen.* 167 (1998) 31.
- [7] D. Klvana, J. Delval, J. Kirchnerova, J. Chaouki, *Appl. Catal. A: Gen.* 165 (1997) 171.
- [8] M. Alifanti, R. Auer, J. Kirchnerova, F. Thyron, P. Grange, B. Delmon, *Appl. Catal. B: Environ.* 41 (2003) 71.
- [9] H.M. Palmer, C. Greaves, M. Slaski, V.A. Trofimova, Y.M. Yarmoshenko, E.Z. Kurmaev, *Physica C* 291 (1997) 104.
- [10] P.R. Slater, C. Greaves, *Physica C* 223 (1994) 37.
- [11] M. Machida, K. Ochiai, K. Ito, K. Ikeue, *J. Catal.* 238 (2006) 58.
- [12] G.H. Lander, P.J. Brown, C. Stassis, P. Gopalan, J. Spalek, G. Honig, *Phys. Rev. B* 43 (1991) 448.
- [13] H.C. Yao, H.K. Stepien, H.S. Gandhi, *J. Catal.* 67 (1981) 231;
K. Wilson, C. Hardacre, R.M. Lambert, *J. Phys. Chem.* 99 (1995) 13755;
A.F. Lee, K. Wilson, R.M. Lambert, C.P. Hubbard, R.G. Hurley, R.W. McCabe, H.S. Gandhi, *J. Catal.* 185 (1999) 491.